

KERALA AGRICULTURAL UNIVERSITY B.Tech.(Agri. Engg) 2016 Admission VI Semester Final Examination-June 2019

Dairy and Food Engineering (2+1)

		Marks: 50
I		Fill up the blanksTime: 2 hours(10x1=10)
	1	The removal of water from a food material by sublimation from a frozen state to the
		vapour state is known as
	2	Stoke's law is used to find out
	3	In spray dryer, powder particles are separated by
	4	The atomizer suitable for materials containing suspended solids is
	5	CIP stands for
	6	Freeze drying is directly proportional to
	7	In uperization, the product is heated to final temperature for a time of
	8	The operating pressure for ultra filtration is
	9	The cut off moisture content between constant and falling rate of drying is called
	10	Time-temperature requirement for in bottle sterilization of milk is
II		Write Short notes on any FIVE of the following (5x2=10)
	1	Factors affecting the drying capacity of drum dryer
	2	Electro dialysis
	3	Regeneration efficiency
	4	Clarification
	5	Flow diversion value
	6	Food properties in relation to evaporator performance
	7	Atomization
		Answer any FIVE of the following. (5x4=20)
III	1	
	2	Describe the construction and working of rotary can washer with neat diagram With the help of a graph, explain the constant acts drains paris doubt full
	4	With the help of a graph, explain the constant rate drying period and falling rate drying period.
	3	Membrane processing.
	3 4	Factors affecting cleaning effectiveness.
	4 5	Explain homogenization with diagram

- 5 Explain homogenization with diagram.
- 6 Different feeding arrangements in evaporator in detail.
- 7 Calculate the rate of movement of fat globule in a centrifugal separator with dia of fat globule 5 μm. Radius of bowl is 12 cm, speed is 6000 rpm. Capacity of separator is 3000 *l*/hr, volume is 3 litre and viscosity is 2.12 centipoise.

P.T.O

Answer any ONE of the following

1 With the help of process layout explain briefly the production of butter

2 Milk is being concentrated from 17% to 52% Total Solids in a vacuum pan. The steam is supplied at 115°C and a vacuum of 66 cm of Hg is maintained in the vacuum pan. The feed to the vacuum pan is 3000 kg/hr at 50°C. The condensate leaves at condensing temperature and the product is assumed to have negligible elevation of boiling point. The specific heat capacity of feed is 3.9 kJ/kg°C and that of the product is 3.5 kJ/kg°C. Overall heat transfer coefficient is 2300 W/m²°C. Calculate

(1x10=10)

(a) Steam consumption

(b) Steam Economy

(c) Heating surface area

IV