KERALA AGRICULTURAL UNIVERSITY

B.Tech.(Agri. Engg) 2016 Admission IV Semester Final Examination-July 2018

Fape.2203

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II

Heat and Mass Transfer (2+0)

Marks: 50

Time: 2 hours

A	Fill in the blanks. $(10x1=10)$
1	Free convection is the result of motion of fluid due to
2	is highest thermal conductive material.
3	Conductive heat transfer thermal resistance in case of cylindrical surface can be obtained using
	the relation
4	The unit of diffusion coefficient is
5	The incident radiation distributed uniformly in all direction is called
В	State True/False
6	Radiation heat transfer cannot take place in the presence of any medium
7	Thermal conductivity of gas increases with the increase of temperature
8	Transmissivity of opaque body is unity
9	The value of LMTD for counter flow heat exchanger is higher than parallel flow heat
	exchanger
10	Effectiveness of heat exchanger can be greater than one (ϵ >1)
	Write short notes on ANY FIVE (5x2=10)
1	Significance of thermal diffusivity in heat transfer?
2	Effect of contact resistance in conductive heat transfer?
3	Why it is advisable to use log mean temperature difference instead of arithmetic mean
	temperature difference to evaluate the performance of a heat exchanger?
4	Importance of fouling factor in design of a heat exchanger?
5	Why critical thickness of insulation is relevant only for curved surfaces? Why not for plane
	wall?
6	What is the difference in emissivity of black, gray and real bodies?
7	Define Wien's displacement law.

Estimate the diffusion coefficient for ammonia in air at 25°C temperature and one atmospheric 1 (5x4=20)pressure. Consider molecular weights as 17, 29 and molecular volumes as 25.81 cm³/gm mole, 29.89 cm³/gm mole, respectively for ammonia and air.

- What do you understand by the term Thermal Boundary Layer? How Prandtl number affects 2 thermal and hydraulic boundary layer for a hot surface?
- Define radiosity and irradiation. Also derive the relation between radiosity and irradiation for a 3 non black opaque surface. 4
- Consider atmospheric air at 25°C in parallel flow at 5 m/s over both side of 1m long flat plate maintained at 75°C. Determine the boundary layer thickness and heat flux at the trailing edge. Consider for Air: $\rho = 1.085 \text{ kg/m}^3$, $\nu = 18.2 \text{x} 10^{-6} \text{ m}^2/\text{s}$, k = 0.028 W/m.K, Pr = 0.707 and $Nu = 0.332 \text{ Re}^{1/2} \text{ Pr}^{1/3}$: 5
- Determine whether it is safe to store a radioactive waste that generating 0.5 MW of energy per unit volume in a hollow spherical vessel of Lead having 0.50 m inner and 0.60 m outer diameter. The lead vessel is further covered with another spherical vessel of Steel having 0.62 m diameter. The whole vessel is surrounded by a fluid of 10 °C temperature having convective heat transfer coefficient as 500 W/m² K. Assume, melting point of Lead as 330 °C, thermal conductivity of lead and steel as 35.3 W/m K and 15.1 W/m K respectively.
- Determine the overall heat transfer coefficient for liquid to liquid heat transfer through a 0.003 6 m thick steel plate [k = 50 W/m.K] for given fouling factor and heat transfer coefficient as $h_i =$ 2.5 kW/m^2 , $h_0 = 1.8 \text{ kW/m}^2$, $R_{fi} = 0.0002 \text{ m}^2$.K/ W.
- A very long copper rod 20 mm in diameter extends horizontally from a plane heated wall 7 maintained at 100 °C. The surface of the rod is exposed to an air environment at 20 °C with convective heat transfer coefficient of 8.5 W/m²-deg. Workout the heat loss if the thermal conductivity of copper is 400 W/m-deg. Also estimate how long the rod be in order to be considered as of infinite length.

IV Answer any ONE of the following

(1x10=10)

- Derive the expression for effectiveness of a counter flow heat exchanger in terms of capacity 1 ratio (C) and NTU. Also enumerate the assumptions made for this derivation and draw a plot between effectiveness and NTU.
- Explain Fourier's Law. Derive the three dimensional Fourier Conduction Equation. 2
