UTILIZATION OF " SALVINIA MOLESTA " / i *f y t lc a n p a y a l)* **FOR BIO - GAS PRODUCTION**

By S. SOMASHEKAREN NAIR

THESIS

Submitted in partial fulfilment of the requirement for the degree of

Master of Science in Agricultural Engineering

Faculty of Agriculture Kerala Agricultural University

Department of Agricultural Engineering COLLEGE OF HORTICULTURE Vellanikkara - Trichur

DECLARATION

I hereby declare that the thesis entitled "UTILIZATION OF SALVINIA MOLESTA (African Payal) FOR BIO-GAS PRODUCTION" is a bonafide record of research work done by me during the course of research and that the thesis has not previously formed the basis for the award to me of any degree, diploma, associateship, fellowship or other similar title of any other University or Society.

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Vellanikkara, $10 \rightarrow 3 \rightarrow 1983.$

SOMASHEKAREN NAIR. S.

CERTIFICATE

Certified that the thesis entitled "UTILIZATION OF SALVINIA MOLESTA (African Payal) FOR BIO-GAS PRODUCTION" is a record of research work done independently by Shrl, S. Sonaghekaren Nsir, under my guidance and supervision and that it has not previously formed the basis for the award of any degree, diploma, ossoclatedhlp or fellowship to him.

Vellanikkara **i o—>-1983**

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CERTIFICATE

We, the undersigned members of the Advisory Committee of Shrl. S.Somashekaren Hair, a candidate for the degree of Master of Science in Agricultural Engineering agree that the thesis entitled "UTILIZATION OF SALVINIA HOLESTA (African Payal) FOR BIO-GAS PRODUCTION¹ may be submitted by Shri. S.Somashekaren Nair, in partial fulfilment of the requirements for the degree.

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I

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SOMASHEKAREN HAIR, 8,

Pedicated

to the memory of Pate Br. Jose Samuel $\frac{1}{\sqrt{2}}$. **Former Professor and Head** Department of. Agricultural Fugineering, Ferala Agricultural University

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Introduction

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Energy Is available abundantly in and around the world we live in. In spite of the enormous quantities of energy nature has given U3, we are now running short of this essential commodity. Of the energy resources available at present fossil fuels and forest wood are quickly getting exhausted. Oil and gas wells are being drained at an alarming pace. Safety r **risks and restricted availability of uranium are the drawbacks for the production and utilisation of nuclear energy. At the same time the fuel price has skyrocketed to a point beyond the reach of the developing world. In short, now we are right in the middle of the greatest crisis of this century, the energy crisis.**

In the recent past, in view of the crisis **ahead, search and research for alternate sources of energy has attracted considerable attention throughout** the world especially in third world countries. Sun, **wind, water, and bio-gas are the fields of special** interest in this connection. The main hopes of **achieving self sufficiency in the energy needs of the** remote rural mass lies mostly on alternate sources of

energy and blogos in particular. Stoner (1976) has identified methane generators as the source of energy capable of meeting a significant portion of our energy requirements in the coming years.

Utilisation of agricultural waste as the raw material for bioga3 production has got innumerable advantages litre easier availability and reduced input cost, in addition to providing an additional income to the farmers. Solar energy panel of National Science Foundation/National Aeronautics and Space Administration believes that by the year 2020, cent per cent of our gas needs will be met by biogas generators based on agricultural waste materials.

Agricultural wastes capable of serving a3 **raw material for bio-gas production may derive from many a source. If this waste derives from a material which hinders cultivation^practices, it will be dual boon i .e . bio-gas production and a solution to the cultivator's problem. From this point of view, salvinla, a serious aquatic weed of common occurrence throughout the world, demands our inraediate attention.** Though water hyacinth also falls within this category, due to its restricted spread and availability, its importance as a raw material for biogas production is practically limited in Kerala.

Infestation of Salvinia molesta, a noxious floating type aquatic weed of common occurrence throughout the world, is particularly severe in tropicel and sub tropical regions. Tho warm inland waters and the increasing number of man-made lakes and water ways foster the growth and spread of this weed. The salvinia genus ranks one among the ten most widely spread aquatic weeds in India. While its presence has been noticed in more than sixty districts in the country, interestingly, tho two State3 most affected by this weed are Kashmir in the Eorth and Kerala in the South.

The species Salvinia molesta, locally known as "African Payal" has spread in enormous quantities during the last 25 years in Kerala. The weed has by now occupied the inland water surfaces of virtually all districts of this Btate. Being capable of prolific growth and rapid multiplication, the weed spreads like an extensive carpet over large aroas of water bodies in the course of a few months. This injturn obstructs

inland navigation, fresh water fishing and other hydrological features. In the Kuttanadu region and the kola lands of Trlohur where the infestation Is the heaviest In the State, thousands of hectares of cultivable lend have been affected by this dreadful weed. Even the daily lives of people in this region. **fffis** who depend on water for domestic consumption, have been affected adversely. The removal of this weed from water can be done manually as well as mechanically. The cost of harvesting this aquatic weed can be offset by utilisation of these plants for biogas production which Inturn may aid to solve our energy problems.

None of the earlier workers have taken up detailed studies dong theselinos. Therefore, the theme of this thesis la a novel approach to find out the feasibility of salvinia for biogas production. The present investigation was undertaken with the following objectives.

- 1. To study the gas production characteristics of . salvinla by simple fermentation techniques in the laboratory utilising small samples of the materials,
- 2. To study the influence of physical conditions of the raw material on the gas production.

- 3*i; To study the gas production under different mixtures of raw material including cowdung as one of the components.
- $4.$ To arrive at a practical combination of working material and environmental condition for optimum gas production from salvinia.
- 5. To design, fabricate and test pilot plant units with a view to test tho reproducibility of laboratory results and to evolve a design of a proto-type salvinia biogas plant.

 $6.$ To evolve a biogas, design which could be used as household/community biogas plant based on the p ilot plant study.

Plant₋

7. To fabricate/adapt existing gobar units to suit the above design and to tost them.

Review of Literature

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REVIEW OP LITERATURE

Salvinia has bocoma a burning problem of the day in the sense it is a devastating weed in cultivators field, a hinderence to navigation and a hurdle to fish culture. Ways and means to find effective and economic utilization of this bane may be the boon we waited long. Scanty literature is available on the economic utilization of Salvinia as a mulch, organic fertilizer, and as the base for hardboard preparation. Utilization of salvinia for bio-gas production Is a novel Idea, which may be of immense and Immediate importance to our cultivators and rural masses. The work done in this line is very limited and so is the case with the relevant literature available at present. Therefore, an exhaustive review on the occurrence, biology, properties, utilization of salvinia, the bio-gas generators, conditions for bio-gas production and the bio-gas production characteristics of cowdung and. water hyacinth is attempted in the following sections.

2.1 Occurrence, biology, properties and utilisation of salvinia

2.1.1 Occurrence

The weed Salvinia is a free floating nonflowering plant coming under the family Salvinacese. Until recently, the species occurring in the fresh water bodies of Kerala and those in many Aslan and African countries, was described as Salvinia auriculata Aubl. It has now been identified to be a distinct taxon named Salvinia molests Mitchell. Although, locally known as "African Payal", this sterile water fora Is actually a native of South America and is probably of horticultural origin (M itchell, 1973a).

Studies in this line by Joy (1978) revealed that specimens of some of the species of salvinia were present in the Botanic Garden at Rio do Janeiro, South America, in 1941. As a weed Salvinia molesta was noticed widely when it invaded the Kariba Reservoir (Africa) in 1959. Mitchel (1974a) reported that salvinia occupied as much $1,000$ sq.km. (21.5 per cent) of water surface in the lake. This might have been a possible reason to call this weed as African Payal (Varghese, 1974).

I Scuthorpe (1987) and Robson (1976) have chronicled *the* distribution of this weed in the tropical

and subtropical region of the world including Africa, Sri Lanka, India, Indonesia, Malaysia and even Australia. In a survey conducted with the help of a **f** quastionnoiro which received information from a total o f **30** States/Dfolon Territories, Varshnoy and Singh (1976) observed the presence of salvinia as a troublesome aquatic weed in some 20 districts in the country. The survey also ranked salvinia as one among the ten most widely spread aquatic weeds (Appendix I).

2.1.1.1 Infestation of salvinia in Kerala

Little is known of the precise mode of origin of salvinia or of tho agents and environmental factors which facilitated its subsequent spread in this State. Cook and Gut (1971) reported that though there was lack of evidence, it was quite likely that the salvinia in Kerela came from Sri Lanka and was first noticed in Kerala as a pest during the year, 1964. But according to George (1976, 1977) the plant, unknown in Kerala before 1953, is believed to have been brought to Trivandrum from Bangalore for botanical studies. It was possible that a few discarded plants, accidently introduced into the Chakkai Canal and Veli Lake near Trivandrum, survived and multiplied beyond all expectations. The weeds rapidly spread from here to other areas

in the State by about 1960 . Also, according to Thomas (1976, 1977, 1979), Salvinia was first noticed as a weed as early as 1956 itself. During the course of an extensive survey of the vascular flora it was observed that the weed was seen in paddy fields, small ponds, canals, and lakes in association with other free floating plants such as Eichhornia and Pistia. Whatever may be the origin, during the last two and α half decades Salvinla molests has spread to most of the $50,000$ ha of paddy fields in the Kuttenadu region and about 10,000 ha in the kole lands of Trichur district (Varghese, 19741 Joy, 1978). The survey conducted jointly by the Kerala Agricultural University and Calicut University during 1977-78 has showed that salvinia io present throughout the low land areas of the State amounting to about 7150 sq.km. (18.4 per cent of the totnl area). She weed is generally absent or has not adversely affected the ponds and paddy fields in the northern districts and in the elevated regions like pathenamthitta and Nedumangadu Taluks of the State. (Calicut University, 1979; Thomas, 1970). The State Department of Agriculture has estimated that during the peak period of infestation between December to May the area of water surface covered by this weed in the whole

State was around two lakh ha (Mathew, 1980). Samuel (1980) had made a more conservative estimate in assessing the area requiring removal of the weed to be of the order of one lakh ha for the entire State.

2.1.2 Biological properties **2.1.2.1 Morphology**

The plant body of Salvinia molesta consists of a slender horizontal stem which bears a pair of heart-shaped floating leaves end an epical growing point $(71g,1)$. From each node hangs a third finely dissected submerged leaf. Salvinia molesta differs markedly from other aquatic vascular plants in fact that it has no roots. It is the submerged leaf which absorbs water and nutrients performing the function of the absent roots. In addition it also acts as a stabiliser (Sculthorpos 1967). Salvinia molesta Is distinguished within the salvinia curiculata group by the presence of long straight chains of sessile to subsesile sporocarps. one mm, or less in diameter, containing mostly empty sporangin (Joy, 1978).

2.1.2.2 Reproduction

Salvinia molests is notorious for its extremely high rate of vegetative propagation.- *Tho* fragile sterna

FIG: 1- TERMINAL PORTION OF A SALVINIA PLANT-

are easily broken, even a violent disturbance of water by rapid currents or strong winds shatters the plants body into many fragments. Any of these detached fragments of the stem bearing one or more breds is capable of growing into an independent plant (Soulthrope, 1967? Mitchell* 1976).

In fact, in all salvinia species, fragmentation and regeneration are more prevalent than sexual development. Propogules (Loyal and Growal, 1966) and Mitchell (1970) showed that Salvinia molesta (cited as S_{\bullet}) auriculata) is incapable of forming viable spores and as such does not reproduce sexually.

$2.1.3$, Growth phases

Salvinia molesta can survive for long periods even under unfavourable conditions. The plant is able to survive fluctuations in water level and in the right conditions will recover rapidly from a prior period of adversity. Hattingh (1961) described three stages of development of salvinia in lake Kariba (1) Primary stage (2) Secondary stage, and (3) Tertiary stage. The primary stage is generally found to be near the shore line where sufficient space is available for horizontal expansion. In this stage, tho plant is characterised

by long internodes and floating leaves which are more or less rounded and quite amall. about 10 mm in diameter (Fig.2). Within a few weeks, the plant usually exhibits the secondary stage in which the floating loaves become larger in size (about **23** mm) in length and 28 man width and partly folded into a keel shape. The internodes still remain long. In the tertiary phase the terminal buds form compact in nature and almost vertical in orientation. Hie leaves are found to be acutely folded ones, broader than they are long, measuring about 23 to 25 ma in length and upto 38 mm in width. Shis is the "mat form" and normally the only stage to bear sporocarps. The transition from primary to tertiary stage takes place in as little as two to three weeks in a suitable habitat (Sculthorpe,1967).

Cook and Gut (1971) distinguished four district phases during the growth of salvinia in a locality $(F1g.3)$. During the first $(intd.1)$ phase, the salvinia is in the primary Invading fora which possibly includes ** all three stages described by Hattingh (1961). But, when no more space is left for horizontal spread, the leaf alters its position, to a more or less vertical one. The salvinia then starts to grow vertically and to build upon its own dead material. This is the second growth

FIG: 2- THREE GROWTH STAGES OF SALVINIA MOLESTA (HATTINGH, 196)

Fig. 3. Four growth phases of Salvinia molesta **(Cook & Gut. 1971)**

phase during which the plants become very large. This phase also cannot go on indefinitely. Due to the massive deposit of dead litter, the selvinia weed is not able to obtain the large quantity of water needed for its growth. The habitant is thus changed and is now ready to be colonised by other plant species. Eie initial colonisers are meatly herbaceous plants which creep over the mats of salvinia and bind them together. \le This is the third phase. The herbaceous plants which creep over the mats of salvinia and bind them together. \times This is the third phase. The herbaceous plants also contribute litter which is deposited on the island providing a suitable habitat for woody shurbs which will. in turn, be eventually replaced by trees. Shis is the fourth phase.

Most habitats in Kerala are either in the first or in the second phase of growth described by Cock and Gut. They do not get a chance to grow into the third phase as the weed® are periodically washed away by flood waters. However in isolated water bodies the third phase of growth is commonly seen. We have little information of the weed having grown into fourth phase anywhere in Kerala. If the weed infostation is not controlled effectively in the near future it is likely

that even the fourth phase will have to be confronted in the State.

2.13.1 Growth rates of salvinia

Growth rates In plants can be assessed by different means. **2**ho application of growth analysis techniques (Evans, 1972) and the concept of doubling rate are considered to be more appropriate for mobile plants like salvinia than the method of net productivity (Penfound and Earle, 1948), commonly utilized in the case of attached plants (M1tchell, 1974a). Several authors have utilised the doubling time techniques in reporting the growth rate of aquatic weeds. Doubling time is the time teken for the material present to double itself. During the analysis of growth of Salvinia molesta. Mitchell (197 $4b$) found that the growth rate of the weed was of exponential form. Gaudet. (1973) working with Salvinia minima and Salvinia molesta under standard culture conditions in laboratory, calculated doubling time in days for numbers of leaves using the formula.

Doubleling time (T)

\n
$$
= \frac{\log 2}{\log N2 - \log N_1}
$$

Where

 $N_{\rm d}$ $=$ Initial number of leaves N_{0} = Final number of leaves t a Observation time

The doubling time (T) of Salvinia molesta vas found to be 4.6 days. But, the growth under field condition was not as rapid and mean relative growth rates ranging between U**-.85** and **8*61** per cent per day in terms of leaf number were obtained. The relative growth rate was increased with increase in light intensity end nutrients. The optimum temperature for the growth was found to be 30° C for both species.

2 *14.Mechanical properties

It Is essential to have a knowledge of the physical/mechanical properties of aquatic weeds, before attempting to design a processing equipment.

With regard to water content, a typical figure of **92** per cent by weight is believed to be present in all aquatic plants with eight per cent as the solid matter content (Little, 1968). This low level of solid matter **S**has been the major deterrent in the commercial utilisation of aquatic weeds. The presence of air in the

order of **70** per cent or nore by volume in the foliage of all free floating plants makes them sufficiently buoyant. A chemical analysis of salvinia conducted by Williams (1956) revealed the following result (Table 1),

Table **1** Percentage matter content in salvinia

A recent study by Thomas et al. (1976) on Salvinia molasta based on samples collected from Trichur, Ernakulam and Kottayam Districts of Kerala also showed a value of **10.1** \pm **0.21** per cent of dry matter (oven dried) content in the weed. However, studies made by tho Department of Life Sciences of tho Calicut University (Xgnatlous, 1979) snd the Department of Agricultural

Engineering of the Kerala Agricultural University (Samuel et al., 1980) indicated that salvinia weed contains only less than five per cent solid matter. Shis show that the moisture content of fresh salvinia would be in the order of 90 to 95 per cent. They also indicated the vast potential for reducing both the volume and weight of the harvested material by the expulsion of water end air in the course of any processing. Livermore et dl . (1971) reported that in the case of water-mil' foil, it had been possible to reduce about **50** per cent of the original weight by an application of pressure equivalent to 2 kg/cm^2 .

Another important physical property of aquatic weeds is their density characteristics. Two common methods of expressing density employed by the Biologists are (**1**) Biomass and (**2**) standing crop estimate (Sculthorpe, 1967). The biomass is defined as the total ness of the plants per unit area expressed on dry weight basis. The standing crop estimate, on the other hand, gives the weight per unit area of the harvested portion of the plant only. With regard to the biomass of salvinia, Eutshi and Vass (1976) found that it varried from $15 - 35$ g/m² during the initial growth

stage. The highest range of values reached was 266 to 32^{h} g/ m^2 on dry weight basis while the ash content of the plant varied from 6 to 16 per cent. Kaul and Usha - Bakya (1976) got similar values of biomass for salvinia (Table **2**) in which the Influence of growth stage was found to be most pronounced.

Period \bullet	Light condition	Average biomass g/m2
May 1973	Partial shade	33.0
	Exposed	30,6
September 1973	Partiel shade	$335 - 1$
	Exposed	326.2
λ		

Table 2 Biomass values of salvinia (Kaul and Ugha Bskya, 1976). l.

Samuel (1972) introduced a new term 'spread density' which was defined as the weight of the imadiately harvested material per unit area. Preliminary experiments made in the College of Agriculture, Vellayoni, Trivandrum by Samuel and Jacob (1977) showed that for salvinia weed which had completed horizontal expansion Just to cover the water surface, the spread density was

of the order of 3 kg/m². When there was no room for horizontal expansion and secondary growth was about to start, the value went upto 7.5 kg/m². With the secondary growth of creepers over the salvinia canopy, the spread density was found to be **12.5** kg/m2.

Bruhn et al. (1971) and Aboaba (1972) studied the mechanical properties of the aquatic weed, water m11.foil (Myriophyllum spicatum) in detail. The relationship among the applied pressure moisture content. dwell time (holding time) end density of the resultingmaterial was investigated. The bulk density (lbs per cusin) of the plant was derived as follows:

> ra = <u>Wg</u> = <u>We Www = W (100 - M</u>) = \mathbf{v} \mathbf{v} \mathbf{v} \mathbf{v} \mathbf{v} *H. (1 0 0 - F- t P . I) 100 V*

whore,

Consolidation testa wore performed to determine the compression properties of the aquatic vegetation. The weight and volume of the material were reduced by applying external pressure utilising a press. These tests provided a means of approximating tho permeability values from the rate of flow of liquid for ya given pressure gradient. The tests provided two other important physical properties also. They were (1) compression index, (Cc) which indicated the compressibility of the specimen and (2) the coefficient of consolidation. Cy which indicated the rate of compression under a given load increment. A value of 0.8 for Cc was obtained for the aquatic weed, ItrrlophyHum spieatum. This value was high compared to that of clay where the Cc value varied between 0.1 to 0.3 .

2.15 Economic aspects

. Floating mats of vegetation may be composed of either pure colonies of a single free floating species or nixed sudd communities of free floating and emergent plants. They in turn produce far-reaching biological and economic consequonces (Soulthorpe, 1967). Holm <u>et al</u>. (1969) reported the difficulties caused by

aquatic weeds In various parts of tho world, while lit t le <**1966**, **1969**) and Mitchell (1973) listed toe problems caused by the weeds in man - made lakes.

Though, actual estimates of losses due to aquatic weeds are not available, weed problems In India were efficially recognised as early as in 1921 (Kulshopadhyay and Sharaphdar, 1976). The problems caused by common aquatic weeds in the country as a whole on the basis of an all India Survey conducted during 1973-71* were listed in order of importance by Vorshney and Singh (1976) as follows:

- 1. Covering of Impounded waters,
- 2. Hindrance to fisheries.
- 3. Choking growth of cultivated plants,
- if. Choking of flowing waters.
- 5. Making water unpalatable.
- **6**. Increased loss of water.
- 7. Creating disease problems.
- 3. Impediment to navigation.
- 9. Hindrance to aquatic sports.

In most areas in Kerala, salvinla has become so well established that other floating plant populations have dwindled out considerably. The first and foremost

of the manifold effects, is the direct mechanical ' hindrance to inland navigation (Thomas, 1979). Any ' 1 i traveller by motor boat from Alleppey to Kottayam, of one of the crew frequently diving into the water and clearing weeds struck in the propeller (Jayakumar, **1980**). Another serious problem caused by the infestation of \cdot salvinia is the severe crop failure in paddy fields of the rice bowl of Kerala (George, 1977). If the fields are left fallow for some months, the unchecked spread of the weed may result in exorbitant costs for its clearance or necessitate complete abandonment of the land. Reports also showed that aquatic weeds might maintain a reservoir of pathogens that are harmful to rice plants (Joy, 1978). Fresh water inland fisheries / have always been an important source of animal protein in le ss **1** developed countries. **2**he blanket of weed offers a direct threat to the establishment of commercial inland fisheries, because of the creation of a shallowwater environment which is both unsuitable for fish to breed in and for fishing boats and nets to be moved salvinia in Kerala have been those of making water which is a popular route, will be baffled by the η ight; which several instances have been reported from Kuttanadu. about. Other important effects of excessive growth of λ

unpalatable, promoting the menace of epidemic diseases, hindering hydroelectric and irrigation schemes and reducing recreation facilities.

2.1.6 Utilization

The idea of offsetting the cost of harvesting the aquatic weeds by finding some ways of utilising the plant material has been the main impetus for the development of several weed processing systems (Livermore and Winderfinch, 1969). Sculthorpe (1967) suggested various methods of utilisation of the plants for horticultural, medicinal and other commercial purposes. Boyd (1972) end national Academy of Sciences (1976) further reviewed these utilisation techniques for aquatic weeds. They included such specific uses as mulches in Garden lands, for compost making and as livestock feeding materials in agriculture and for purification of industrial waste, as packing material and as pulp for paper making in industry as well as in generating biogas for energy production. As in the case of other aquatic weeds, it has been found that salvinia can be effectively utilised as an organic fertiliser. The trials at the College of Agriculture, Vsllayani, indicated that '■5 ccopost made of salvinla in rich in plant nutrients *A* (Joy* **1978**). Salvinla can also be used aa a mulch in

coconut or cocoa garden as is being practised In Ceylon (Menon, 1971). The use of this weed is already contemplated by some industries in Kerala as raw material for hardboarde and **as** a packing material for delicate articles like glass wares (Thomas, 1979). It is stated that aquatic weeds might also one day provide a new source of energy for Kerala. Laboratory and pilot plant level studies have also brought out the tremendous potential for biogas generation from the harvested salvinia weed mass (Samuel et ell_0 , 1980 .

2.2 Bio-gas generators

The first attempt to build a digester to produce methane gas from organic wastes (cowdung) was mad© in Bombay, in 1900. The problem to obtain a cheap fuel and fertilizer at a local level, by Indian Agricultural Rosearch Institute in 1940 led to the basic chemistry of anaerobic decay. In the 1950*s simple digester models were developed which ware suitable for village homes. More ambitious designs were tested by the planning Research and Action Institute in the year $1950.$ The success of it led to the start of the Gobar Gas Research Station at Ajitmal (Stoner, 1976) and a 10 HP engine working on bio-gaa havo been developed there.

 $27\,$

In 1950, Jashbhari Patel made the first breek through in the manufacture of a practical plant. He named his plant *Gramalaxmi* Gas plant (Sathianathan, 1975). By 1961 Kadhi and Village Industries Commission (KYIC) included gobar plants in its programme and an improved typo of Gramaloxmi model was adapted and the introduction of the K.V.I.C. model was done.

Many research conducted at many parts of the country contributed new models of biogas plants such as Jenatha biogas plants, T.N.A.U,model biogas plant, Smgyolekshmi model, etc.

Janatha biogas plants were constructed in many parts of India, and vide publicity is being given for it all over India by the Directorate of Extension, Ministry of Agriculture and Irrigation. T.N.A.U. models are popular in Tamil Nadu and was developed by the Tamil Nadu Agricultural University. The Huagyalekshmi plant was developed by tho Indian Institute of Agricultural Sciences, Bangalore. **1** Newly a low cost biogas plant has been developed by A.M.M. Murigappa Chettiar Research Centro, Madras using low density polythene dome (Anon, 1982).

2.3 Biogao production characteristics of cowdung and water hyacinth.

The studies conducted by Sriramulu et al. (1980)

to determine the moisture content, total solids, vola tile solids and gas yield in terms of V.S,reported the following data according to the Table **3**.

Table **3**. Comparison of water hyacinth with cowdung.

Some work conducted by Guha et al. (1976) in which the gas production characteristics of cowdung and water hyacinth were compared reported that in the case of water hyacinth the rate of evolution of gas **a *** is maximum on **6**th - **9**th day whereas in cowdung the maximum gas evolution is on the 14th - 16th day.

According to the Tamil Nadu Agricultural University, Coimbatore the quantity of gas required for different purposes, are as follows:

- 1. Domestic cooking \sim 2 Cu.m./day for 5 members
- 2. Water heating \sim 3 Cu.m./day for 100 L
- $3.$ Lighting $-$ 0.10 to 0.15 Cu.m/hr.for each light point.

2.4 Conditions for improved biogas production 2.M-.1 Anaerobic digestion

The process of conversion of organic compounds into methane consists of the following steps.

The "anaerobic" bacteria responsible for digestion cannot survive with even the slightest trace of oxygen. So, because of the oxygen in the substrate which is fed to the digester, there is a long period after loading before actual digestion takes place. During this initial "aerobic" period, traces of oxygen are used up by $oxygen - Ioving bacterial$, and large amounts of carboodioxide are released.

Die aneroblc phase includes a serioa of reactions by several kinds of anaerobic bacteria feeding on the raw organic matter.

In the first stage of digestion, organic material which is digestable (fat, protein, and starches) are broken down by acid producing bacteria into simple

 $\frac{1}{\epsilon}$

compounds. This phase is termed hydrolysis. During this phase the complex materials are converted Into simpler substances (especially volatile acids). The most important volatile acid is acetic acid. About 70 per cent of tho methane produced during fermentation comes from acetic acid (Acid phase).

Once the raw material has been liquefied by the acid producing bacteria, methane producing bacteria convert the volatile acids into methane gas. These bacteria are very sensitive to change in the conditions of their environment. The successful digestion depends upon maintaining a balance between those bacteria which produce organic acids and these bacteria which produce methane ga**3** from the organic acids (Stoner, **1976**),

 $2.4.2$ Biogas production under varying conditions of organic material.

 $2.4.2.1$ Effect of drying the substrate

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Some experiment conducted by (Sriramulu, 1980) reported that using water hyacinth as the substrate ^**7**"**5**G LAs of bio-gaa was produced from dried water hyacinth, as compared to 51-6¹ L/kg of gas from green leaf. The studies further reported that by drying the volume of the substrate can very well be decreased.

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so that the net quantity of substrate that can be accommodated in unit volume can be doubled.

2*l>.**2*2** E ffect of temperature

Many studies in this field reported that biotas production has an increased activity at higher temperatures. According to Boshoff (1963) double the gas production was achieved at **32**°C as when compared to gas production at 22° C. Another study showed a 200 per cent increase in the rate of gas production at $h2^{\circ}$ C as compared to the rate at 32 $^{\circ}$ C (Fang, 1973).

2.4.2.3 Effect of agitation

Some studies conducted by Sierp (1931) reported that when the slurry is well mixed an increase of 10 to 15 per cent bio-gas was obtained. The study also reported that agitation could control the scum, sludge, and could release carbondioxide from the slurry.

2.4.2.4 Effect of recirculation

The experiments conducted at national Environmental Engineering Research Institute revealed that, daily gas production doubled when recirculation of the bio-gas was incorporated (Sathianathan, 1975).

 $2.4.2.5$ Effect of pressure

 $\ddot{}$

Very tittle work has been done in the field of effect of pressure on bio-gas production. However some work done by Babbit and Bauman (1958) revealed that the pressure allowed in the slurry should not exceed **15** to **18** cms of water.

Also other parameters controlling this biogas generation are C/N ratio, pH concentration of the slurry etc. The elements carbon (as carbohydrates) and nitrogen (as protein, ammonia etc.) are the chief foods of \mathcal{L} , and the contract of the contract of the contract of the contract of \mathcal{N} anaerobic bacteria. Carbon is utilized for energy a $\mathring{\mathfrak{a}}$ d the nitrogen for building cell structure. These bacteria use up carbon about 30 times faster than they use nitrogen. Therefore the best C/N ratio is considered to be 30 (Stoner, 1976).

The pH of the slurry is another important parameter in bio-gas generators. The optimum pH for most of the bacteria is between 6.5 and 8.0. The acid forming bacteria are sturdy and are known to operate at a pH range as low as 5.5. The methane fermenters are very sensitive to low pH end do not thrive below 6.5, their optimum being 6.8 to 7.2 (Sathianathan, 1975).

I

Being the major aquatic weed, the raw material availability will be greater in the case of salvinia as against water hyacinth or any other raw material. Assuming that an average bio-mas yield of approximately **100** tons/ha, the bio-mass availability is of the order of 20 million tons from about 200,000 ha in the State. Thus it appears that there are insense possibilities for introduction of salvinia biogas plants in Kerala. This in turn can be utilized as a practical measure to partly overcome the fuel energy shortage in the State.

The slurry, i.e. the spent material of the bio-gas plant, also finds application as manure. This inturn can be an added attraction for the popular use of such bio-gas plants in the rural area of the State.

Materials and Methods

MATERIALS AND METHODS

The present investigation on 'Utilization of Qalvinio nolasta (African Payal) for biogas production**1** was undertaken in the Department of Agricultural Engineering, College of Horticulture, YeUanikkara during the period **1981-82** and **1982**- **83*** The materials used and the methodology followed were as follows.

3.1 Materials

Salvinia molaata (African Payal) and water hyacinth utilized for the study were collected from the ponds end paddy fields nearby the University campus. Cowdung was supplied by the Fodder Research Scheme, : College of Veterinary and Animal Sciences, Mannuthy.

The materials like mild steel sheet, drums, G.I.pipes, valves, bends, tubings etc. utilized for the fabrication were purchased from the local market.

3.2 Experimental details 3*2*1 Atmospheric temperature

The atmospheric temperature during the experimental period is furnished in Figure \mathcal{L}_*

3*2.2 Digostable properties of Salvinla molasta

The digestable properties of the raw material **i** used for digestion has got a direct relationship with the biogas produced. Accordingly in order to assess the quality of Salvinia molesta in terms of digestable properties, were assessed as follows.

3.**2**.**2*1** Moisture

The moisture content was determined by drying a sample of salvinia (20 g) in a hot air oven at 105°C, until a constant weight was obtained (Sathlanathan, 1975) end was expressed as percentage moisture. Moisture percentage was calculated as follows. % Moisture a Wt.of fresh sample - Wt.of dried sample

 $\boldsymbol{\mathsf{x}}$ 100 Wt. of fresh sample

3. **2**. **2.2** Total solids (X.S)

The weight of drymatter, remaining after drying as in **3**. **2**.**2**.**1** , was determined as per the following formula and was expressed as percentage total solids (T.S).

 $T_{\bullet}S_{\bullet}$ a Wt. of dried sample **a* a --------------------------------- *X* 100 Wt. of fresh sample

 $3.2.2.3$ Volatile solids (V.S)

She dry material obtained in **3*** **2*** **2.2** was charred over a flame. The charred material so obtained was ignited in a muffle furnace operating at 550° C. After $h \approx 5$ hours, the ignited material was transferred from the muffle furnace to a desiccator and was allowed to cool overnight. The weight of organic solids burned off was determined and was expressed as percentage V.S.

 $3.2.2_*¹$ Fixed solids (F.S.)

Fixed solids of salvinia was calculated from the following expression and was presented as percentage F.S. Percentage fixed solids = Percentage total solids = percentage volatile solids.

3«2*3 Drying of salvinia in direct sun and in shade

Samples of salvinia (400 gm) each was dried under direct sun and shade, spreading on the floor. Sun drying was limited to six hours a day from 10 A_tM_t to 4 P.M. The mean temperature for the period vas 32° (Max.) The drying operation both under sun and shade was carried out for three days. Their weights were recorded at hourly intervals.

$3*2*+$ Gas production characteristics of salvinia and cowdung.

Details of the experiment designed to study the gas production characteristics of salvinla and cowdung under laboratory conditions are furnished below.

Samples of salvinia (350 g each) was taken in ecnicel flask in triplicate. 100 ml. of water and **50** m l.of cowdung slurry was added to the flask. The cowdung alurry served as the inoculam. Anaerobic conditions was provided in the flask by means of airtight corking. It was allowed to ferment for 45 days. The gas formed tinder anaerobic condition inside the flask was collected and measured by water displacement methods. In the case of cowdung 100 g cowdung and 100 ml of water served as raw material cum inoculam mixture. The rest of the procedure followed was the same as in the case of Salvinia.

Detailed outline of the laboratory set up is shown in Figure $5.$

$3.2.4.1$ Gas production of salvinia under varying physical condition

The following three physical conditions were employed.

FIG: 5. EXPERIMENTAL LABORATORY SET UP.

 $\label{eq:2.1} \frac{1}{\sqrt{2\pi}}\int_{\mathbb{R}^{2}}\frac{1}{\sqrt{2\pi}}\int_{\mathbb{R}^{2}}\frac{1}{\sqrt{2\pi}}\int_{\mathbb{R}^{2}}\frac{1}{\sqrt{2\pi}}\int_{\mathbb{R}^{2}}\frac{1}{\sqrt{2\pi}}\int_{\mathbb{R}^{2}}\frac{1}{\sqrt{2\pi}}\int_{\mathbb{R}^{2}}\frac{1}{\sqrt{2\pi}}\int_{\mathbb{R}^{2}}\frac{1}{\sqrt{2\pi}}\int_{\mathbb{R}^{2}}\frac{1}{\sqrt{2\pi}}\int_{\mathbb{$ $\Delta \sim 10^{-1}$ N۳

- 1. Salvinia as a whole.
- Salvinla under chopped conditions (Chopping was done in the mixi using the chopping blade for one minute).
- $3.$ Salvinia dried under sun for two days (21 g of dried material obtained from 350 g of fresh material formed the sample size in this case).
- 3.2.4.2 Gas production of salvinia as influenced by , mixing with other raw materials

The experimental set up consisted of the following combinations.

- 1. Control **a** SaXvlnia (350 g) 4- Water (100 na) + Cowdung inoculam (50 ml).
- 2. Salvinia (175 g) + Cowdung (50 g) + Water (100 ml). (Quantity of salvinia and cowdung was selected such that their dry weights unre in the ratio 1:1).
- 3. Salvinia (175 g) + Water hyacinth (45 g) + Water $(100 \text{ m}.) +$ Incculam $(50 \text{ m}.)$. (Quantity of salvinia and water hyacinth was selected such that thoir dry weights uare in the ratio 1i1),

 $3.2.4.3$ Gas production under different proportion of cowdung with aalvlnia.

Shis experiment to find out the best proportion of cowdung with salvinia (the best raw material combination obtained in 3.2.*t»2) producing maximum gas yield, consisted of the following combination,

- 1. Salvinla end cowdung in the ratio (On dry weight basis) of $1:1$. 1.e. $1/5$ g Salvinia, 50 g cowdung and 100 ml water.
- 2. Salvinla and cowdung in the ratio (on dry weight basis) of 2:1. i.e. 233 g of salvinia. 33 g cowdung and 100 ml water.
- 3. Salvinla and cowdung in the ratio (on dry weight basis) of $142.$ i.e. 116.7 g salvinia, 66.5 g cowdung and 100 ml of water.
- $3.2.4.4$ Gas production from salvinia and cowdung under different dilutions.

E ffect of dilution of slurzy with water was studied and the experimental details are furnished below.

Salvinla and cowdung mixture were taken in the ratio 111 on dry weight basis (Salvinia 175 g and cowdung 50 g, the best combination obtained in 3.2.⁴.3). The dilution treatments employed were as follows:

- 1. Control Salvinia (175 g) + cowdung (50 g) mixture (The ratio-being 111 in terms of dryweight) $+$ 100 ml. of water.
- 2. It varied from the control by the fact that 200 m L of water was added.
- $3.$ It varied from the control by the fact that 450 ml of water was added.
- $3.2.4.5$ Gas production of salvinia and cowdung mixture as influenced by sunlight and shade.

The influence of shade and light was studied by performing the experiment under direct sunlight (the samples were kept on the terrace to ensure the availability of direct and continuous sunlight), and, shade (refers to the diffused light or shaded condition inside the lab),

3.3 Fabrication of biogas plant models for pilot plant studies

The pilot plant studies were based on four models of biogas generators. A new design of biogas plant was made at the Agricultural Engineering Research Workshop, Mannuthy. Its performance was compared with the following models. .

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(1) Maptive design of conventional K.V.I.C.model.

(11) Enagyalekshmi model - Institute of Agricultural **Sciences, Bangalore.**

(iiDHoriaontal KAU model (Jose Samuel, 1981).

All the four model**3** including the newly designed model were fabricated at the Agricultural Engineering ^Research Workshop, Mannuthy, All these models were fabricated In such a way as to maintain uniform capacity of 200 litres. for easy comparison.

3. **3*1** New K.A.U. model

The new model of biogas plant designed at **K.A.U.** s consisted of a square tank having dimensions **6**? cm x h-5 cm x 67 cm (Fig,**6**) and the side to depth ratio of this model was **erne,** ffiiis was made out of 16 gauge mild steel sheet. An arched shape was provided at the top surface, neant for gas collection. A volume of 75000 cm^3 was available for gas collection. The arch or domeshape was intended to prevent the clogging of the gas outlet by the material undergoing fermentation, She gas outlet originating from the top surface of the tank consisted of a bank tube (12*1* mm) fitted with a wheel valve, a reducer, and a P_tV,G_\bullet pipe in serial sequence. The inlet and outlet

FIG: 6 PILOT PLANT NEW KAU MODEL.

previsions of tho tank, meant for feed in and feed **£,vn** out, were made of $7·6.6$, I.pipe. In terms of the vertical height froai the base, the inlet was maintained at a higher level compared to the outlet. The inlet and the cutlet wore firmly attached to the digester by using a bracket.

A partition wall or baffle was provided near to the outlet side. Thereby the maximum exposure of the material for fermentation was achieved.

For easy cleaning a hand^hoie wag provided on the side of the tank. Three thermometer holes were provided at varying heights of the tank in order to measure the temperature and to verify the state of the slurry at different heights.

3.3.2 Adaptive design of K.V.I.C. model

She adaptive design of K,V,I»C.consisted of the following parts (Plate 1 and $F1g, 7$).

1. Digester

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Digester was made, using a oil drum of 91 cm height, 58 cm diameter (diameter to depth ratio equal to 0.63), and of 200 litre capacity. Since the present study included only tho batch digestion process,

Pilot plant conventional K.V.I.C.model Plate I

FIG: 7 PILOT PLANT CONVENTIONAL KVI-C MODEL

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the mixing tank and the partition wall, originally present in the K.V.I.C.model were omitted from the adaptive modal.

2. Gaa holder

The gas holder was made out of a 16 gauge mild steel sheet. The mild steel sheet was rolled to a convenient diameter of 55 cm, so that it could slide Inside the digester tank. The gas holder so made had the dimensions of 36 cm height and 55 cm diameter with a collection volume of 85530 cm^3 .

3» Gas mains

The gas outlet originating from the top surface of the tank consisted of a bent tube $(i27mm)$ fitted with a wheel valve, a reducer and the P.V.C. pipe In serial sequence.

4. Inlet and outlet

The inlet and outlet were made out of ?%cm diameter G.I.pipe and were welded to the digester In such a way that their lower ends Just touch . ; the bottom of the digester. They were placed inclined to the digester. The vertical height of the inlet and outlet were 92 cm and 87 cm respectively.

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3.3.3 Bhagyolokshmi plant

This is a variable pressure bio-gas generator designed by the Indian institute of Agricultural Sciences, Bangalore. *A* pilot plant model was fabricated at the Engineering Research Workshop. This model consisted of the following parts such as digester, inlet and outlet, valve for tapping the gas etc. (Plate 2 and Fig.8),

The digester was fabricated using 16 gauge mild steel sheet. She diameter end height of the digester wers 62 cm and 62 cm respectively (Diameter to depth ratio being 1:1). The inlet and outlet were closely fitted with the digester body. The top of the digester had a dome shape, the capacity of the gas collecting chamber being $60,000$ - cm^3 and the outlet fittings were exactly the same as described earlier (section $3.3.1$). The baffle or partition wall was not included in this model as it was not meant for continuous feeding.

3.3 A Horizontal type K.A.U. model

This variable pressure model was fabricated using a 200 litre oil drum having 91 cm height and 58 cm diameter (Plate 3 and Fig.9) (Samuel, 1981).

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FIG: 9 PILOT PLANT HORIZONTAL TYPE BIO-GAS PLANT

The drum was placed horizontally to serve aa the digester, The inlet was made out of **3**** diameter G.I.pipe with a height of 66 cm from the top of the digester* The outlet of **63.5** cm height (from the top of the digester) was fabricated by providing a cross sectional area of 20 op s 20 cm and was mads of **18** guage mild steel sheet* A hand hole was provided at the top for easy cleaning and loading of the tank. A valve provided at the top of the digester served the purpose of out take of the gas were from the digester. Two baffles provided inside the tank for **Increased efficiency.** However, continuous feeding was not undertaken during the present course of investigation.

3,1* Gas production characteristics of salvinla and cowdung mixture at pilot plant level using different models,

The fabricated pilot plants selected for this experiment were

- 1. Conventional K.V.I.C. model
- 2, Bhagyalekshmi model
- 3. Horizontal K.A.U. model
- H_* New K.A.U.model

A ll these models (Elate *b)* were loaded with 35 kg of salvinla and 10 kg of oowdung. Water was added

sufficiently (about 100 litres) such that the floating drum could very well float over it. These experiments were conducted in the Research Workshop, Mannuthy and the generators were placed in such a way that they could get direct sunlight. Daily observations were made using a glass flow meter. The fermentation period was limited to about 45 days and daily temperature and gas yield were recorded,

3.5 Effect of pressure on biogas generators

The experiment was conducted in order to find out the effect of pressure if any, on the production of biogas. For this experiment three generators of K.V.I.C. model with gas collectors of varying weights were employed. The gas collectors of 10 kg, 25 kg, and 40 kg giving intensities of pressure 4.6 cm, 11.5 cm, 18.5 cm of water respectively were utilised for the study. All these three models were loaded with 50 kg of salvinia, 15 litres of used slurry (as inoculum) and 100 litres of water, so that the floating drum could very well . float over it ensuring the anaerobic condition. The fermentation of the above substrate was allowed to continue for 45 days during which the daily temperature and gas yield were recorded. (Plate 5).

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3.6 Modification and fabrication of the pilot plants

The new K.A.U. model was modified by incorporating a system for the recirculation of bio-gas. The recirculation was achieved by fitting two additional Valves, *A* rubber bladder was Inserted in the piping \therefore between the two valves. A tube was fitted to the second valve. The other and of this tube being opened at the bottom of the tank into the slurry. Recirculation was achieved as follows. The first valve was opened while the second one was kept closed so that the gas can enter the bladder. Then the second valve was opened, keeping the first one closed. The bladder was pressed so that the gas passed through the second valve and then passed through the slurry creating bubbling (Fig, 10 and Plate 6).

Also the conventional K.V.I.C.model was modified by incorporating an agitator. The agitation was effected by rotating the handle attached to the shaft at the top (Fig, 11),

3.7 Comparison of bio-gas generator models

This ©speriment was aimed at comparing the various designs of bio-gas generators. For this purpose the following models were chosen.

Modified pilot plant New K.A.U. model with
recirculation of bio-gas Plate VI₁

1. K.V.I.C.model

2. K.V.I.C. model with agitator.

3* K,A*U.model without recirculation of gas.

b, K. A. U, model with recirculation of gas.

5* Bhagyalekshmi model.

 6 , Horizontal K.A.U.model.

All the above six models were loaded with i 'Banda'a 'Banda'a 'Banda'a 'Banda'a 50 kg salvinia, 15 litres of used slurry (as inoculam) and 100 litres of water and anaerobic condition was maintained. Fermentation was carried out for 45 days. Daily gas yields were recorded using a gas flow meter. Temperature for the whole period was also noted.

3.8 Exploring the feasibility of utilising existing KyiC type Gobar gas plant for blo-gas production , from salvinla

This experiment was conducted in the K7IC type Gobar gas plant, at the K.A.U. Research Station and Instructional Farm, Mannuthy (Plate 7). The capacity of the Gobar gas plant utilised for this study was about two cubic meter with a diameter of 120 cm and having a total height of 210 cm. The floating drum had the dimensions of 100 cm height and 110 cm diameter and was made to float inside the tank. It was loaded with 550 kg of salvinla, 157 kg of cowdung, and enough

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water for dilution and effective anaerobic condition. For 45 days the gas production was recorded using a glas flow meter.

3,9 Design of a prototype unit for household purposes (Using dried salvinis as the substrate)

Let the daily availability of fresh salvinia be $7+00$ ig. If this fresh sample is dried for two days, its weight will be reduced to about $^{10}0$ kg. If equal quantity of water is added to it, the daily input will be 80 kg.

Calculation of *volum* requirement

Daily input w $40 \text{ kg} + 40 \text{ kg} = 80 \text{ kg}$ Input for $45 \text{ days} = 80 \times 45 = 3600 \text{ kg}$ This consists of 1800 kg of water and 1800 kg salvinia. It is estimated that 500 kg of dried salvinia can be **accomodated ii! osie cubic Eater,**

Thereforo, space requirement for 1800 kg = 3.6 cubic meter Space requirement for 1800 kg of water $= 1.8$ cubic meter i Therefore, total space requirement $=5.4$ cubic meter

n£t= 6 cubic mater

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Gas yield from 6 cubic. meter capacity generator

It is estimated (from the previous experiments) that 1 kg of dried payal can evolve 93 litres of gas in *h\$* days, therefore, the gas evolved from *ho* kg of dry payal $=$ 40 x 93 = 3720 litres = 3.7 cubic meter.

Requirements that can be net with the above gas yield

It is estimated that one person requires 0.4 cublc meter of gas per day for cooking purposes and about 0.1 cubic meter of gas for lighting purposes. Therefore the total gas requirements per day for a person will be Q.J cubic meter. Hence this 3»7 cubic meter of gas can be utilised by $7 - 8$ persons for their cooking and lighting purposes.

Results and Discussion

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RESULT AND DISCUSSION

b.1 Digestible and drying properties of salvinia¹ 4.1.1 Digestible properties of Salvinia molesta

The digestible properties of Salvinia raolesta such as moisture, total solids, volatile solids and fixed solids were assessed in order to ascertain its feasibility for bio-gas production. The results of the study are depicted in Table *h.*

Table *h.* Digestible properties of Salvinia molesta

It may be seen from the table that salvinia contained 95.43 per cent of moisture, 4.57 per cent of total solids, 85.9 per cent volatile solids (in terms of total solids) and 14.1 per cent fixed solids (in tern© of total solids).

It Is evident from the data that salvinia, qan be utilised as a potential raw material for bio-gas production, however, in comparison to cowdung (total solids 18,26 per cent) end water hyacinth (total solids 18 per cent) (Sriramulu, 1980), more quantity of salvinia is required for the production of unit bio-gas.

From the figures pertaining to the.volatile solids it may be seen that salvinia (85.9 per cent) has got more volatiles actually activated by the bacteria during the fermentation process, compared to cowdung **(70** - **80** per cent V.S) and water hyacinth : (82.5) per cent $V.S$).

While considering the fact that salvinia occurs as a weed abundantly in paddy fields and ponds the availability and cost is not likely to become a barrier for utilizing it for bio-gas production. Even if it is taken that four kg fresh salvinia is required to get the total solids obtainable from one kg. cowdung or water hyacinth, salvinia could be rated as a cheaper raw material.

4.1.2 Drying characteristics of salvinia

The result of the experiment conducted to determine the percentage reduction in weight of salvinia

by drying it under direct sun and shade is as shown_, in Table 5 and $F1g.12.$

Table 5 Drying rate of salvinia under sun and shade

Period of drying		Weight of the samples (g)	
Days	Time in hour	Sun dried	Shade
$\mathfrak T$	0 123456	400 204 137 137 27 77 60 47	400 330 282 260 213 187 154
11	0123456	3221188 18888 177	1305220265
III	$\boldsymbol{\theta}$ するさらら	17 17 17 17 17 17 17	33335555

From the data it is seen that the weight reduction of salvinla in sunlight is much faster when

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compared to that in shade. A weight reduction of about 61 par cent was obtained in shade drying comparing to 88 per cent in the case of drying in sun in the first day itself. At the end of the second day the net reduction in weight was equal to 95.5 per cent under sun whereas 86 per cent under shade. $\mathfrak{m}_{\mathfrak{p}}$ the third day its weight remain unchanged for sun * drying while a weight reduction equal to 91 per cent in the ease of shade drying.

Thus it is clear that the effect of sun drying for two days is equivalent to drying it in shade for five to six days. It is also evident that drying under sun is faster compared to drying under shade. Thus, drying of salvinia for two days under sun may be recommended to shade drying.

firied salvinia has got specific advantages : over fresh salvinia viz. bulk reduction in transportation and storage, minimum generator volume and better keeping qualities. However the effect of drying- on gas production characteristics of salvinia has to be assessed before taking the final recommendation. The results of tho experiment conducted in this connection are discussed elsewhere $(l_{12}.6)$.

^♦2 das production characteristics of galvinia Gas production characteristics of ealvlnia in comparison with that of coudung.

Eh© gas production characteristics of saLvlnia end cowdung is presented in Fig. 13. Detailed information is given in Appendix II.

It may be observed from the $Fig.13$ that the gas output was negligible for the first five days. 2his negligible or sero production of gas may be due to the lag phase of the incculam (microbes). From the sixth day onwards the gas production started and attained the peak value (112 ml) on the 20th day. Thus it appears that the lag phase of the inoculam was restricted to five days. It was also observed that the major bulk of the gas produced during the period $\mathfrak f$ vom six days to eleven days was carbondioxide* This may be attributed to the aerobic conditions which prevailed and dominated the initial phases. Accordingly the anaerobic break down series , consisting of carbohydrate hydrolysis ------> simple carbohydrate enaerobic acid (acidic through alcoholic osydatlon), butyric acid, propionic acid etc. as anaerobic respiratory produces incthanognes \longrightarrow Methane, carbondinside, might not have functioned during this period. Actual

methane production was observed from the 11th day. During this period the anaerobic phase was dominated. The rate of gas production was found to decrease from the 20th day onwards and it touched the uneconomic level (38 ml) by the 45th day. Whis decline in gas production may be due to the, cumulative effect of the exhausting raw material and the Initiation of the . declining phase of the microbial growth. From these' results it may be possible to formulate a feeding schedule so as to maintain optimum or maximum gas production continuously.

3b tho Gaso of oowdung the lag phase was six days and the log phase (period for maximum gas production after the lag phase was 13 days and the economic period of the gas production was 45 days.

The cumulative gas production for the first 45 days from salvinia was 2569 ml and from cowdung was 3020 ml. Thus the average gas yield was 163.11 ml per kg of salvinia and 191.7 ml per kg of cowdung (670 ml/kg of cowdung = 191.7 ml/kg of salvinia equivalent). This revealed that 7.34 litre of gas is obtained from one kg of fresh salvinia and 8.6 litre from one kg of cowdung for about 45 days.

This in turn is equal to. 160 cubic meter per kg of total solids and 0.187 cubic meter per kg of volitile **I** solids in the case of salvinia and about 0.189 cubic meter per kg of total solids and 0.219 cubic moter per kg of volitile solids in the case of cowdung, all the values being calculated taking the retention period as 45 days.

h«2*2 Gas production of salvinla under varying physical conditions

The effect of physical conditions of salvinia, viz., as a whole, as chopped and as dried, on gas production is portrayed in Table 6 and Fig.14. The details are available in Appendix III.

Table 6 Effect of physical conditions of salvinia on gos production

		Physical conditions of salvinia	
	As whole	Chopped	Dried
Lag period for gas production (days)	6	3	lş.
Period for maximum gas yield (days)	20	1	13
Peak gas produced (ml.)	125	112	78
Cumulative gas production 2569 (ml.)		3111	1935
Cumulative gas production mVkg in $\overline{45}$ days	7孙0	8890	5530
Gas production in m ³ /kg of T.S. (Total solids)	0.160,800	0.195	0.121
Gas production in $m3/kg$ of V.S. (Volitile solids)	0.186	0.226	0.140

It is evident from the data that with respect to the minimum lag period for gas production, cumulative gas production from unit raw material and gas production par unit weight of total solids and volatilo solids, chopped salvinla excelled over the other two physical conditions. The increased surface area may he the reason for the superior performance of chopped aelvinia over whole salvinla* However, the extra energy and labour required for chopping salvinia should he taken Into consideration before making the filial recommendation.

Ihe lesser cumulative gas production recorded by tho dried salvinla may be due to the possible loss of volatile solids during the drying process. However it may be noted that dried salvinia requires lesser generator volume for unit gas production.

In the case of dried salvinia too, energy, labour and space required for,drying appears to be the limiting factors. From the convenience point of view thole salvinla may be recommended for gas production purposes.

b.2*3 Gaa production of Sslvinia as influenced by mixing with other raw materials

Gas production characteristics of salvinia cowdung mixture and salvinia - water hyacinth mixture is presented in Table 7 and Fig. 15. Detailed observation is furnished in Appendix XV,

As it may be seen from the Table, the combination of salvinia - eoudung mixture was the best raw material for the gas production. This combination recorded the best values of all the parameters under discussion. A reduced lag period and early peak gas yield attainment are the observations of special interest. Based on these observations it appears that mixing with cowdung might have added more inoculum end hence an enhanced microbial activity. Thus it may be argued that increased number of micro organisms are capable of bringing down the period for the Initiation of gas production and for achieving an early maximum gaa production. Mixing of water hyacinth with salvinia also showed favourable effects compared to salvinia alone. This favourable effect may be attributed to the easily assimilable constituents of water hyacinth.

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Table 7 Effect of raw material combination with
salvinia on gas production

Gas production under different proportion of cowdung with salvinia

In order to standardise the optimum proportion of cowdung with salvinia for maximum gas production the experiment was performed and the results of this experiment *axe* presented in Table 6 and Fig. 16. Detailed observations ere furnished in Appendix V.

It may be evidenced from the above data that the lag phase for gas production and the period for maximum gas yield remained insensitive to the cowdung proportion, employed in this study. However based cn the cumulative gas yield, gas production per unit total solids and volatile solids, mixing salvinia with cowdung in the ratio 1:1 is found to be the most outstanding. This may be due to the properly balanced substrate to **I** inoculam ratio.

$4.2.5$ Gas production from salvinia and cowdung mixture under different dilutions

It nay be seen from the data presented in Table 9 and Fig. 17 that the raw materiel (salvinia and cowdung) to water in the ratio of 1:1 recorded maximum daily gas yield, cumulative gas yield and gas production per unit total solids. However the lag period for

 $\label{eq:2} \frac{1}{\sqrt{2}}\sum_{i=1}^n\frac{1}{\sqrt{2}}\sum_{j=1}^n\frac{1}{\sqrt{2}}\sum_{j=1}^n\frac{1}{\sqrt{2}}\sum_{j=1}^n\frac{1}{\sqrt{2}}\sum_{j=1}^n\frac{1}{\sqrt{2}}\sum_{j=1}^n\frac{1}{\sqrt{2}}\sum_{j=1}^n\frac{1}{\sqrt{2}}\sum_{j=1}^n\frac{1}{\sqrt{2}}\sum_{j=1}^n\frac{1}{\sqrt{2}}\sum_{j=1}^n\frac{1}{\sqrt{2}}\sum_{j=1}^n\frac{1$

${\tt Table\ 8}$. The effect of different proportion of cowdung with salvinla

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initial gas production remained as five days irrespective of the dilution factor. Any tilt in the ratio cither in favour of substrate or water resulted in poor gas yields. Thus it is evident that the role of water is Halted to dissolving the soluable solids of the raw material and make it available for fermentative break down. Detailed observations are furnished in Appendix VI.

*+•2.6 Gas production of salvinia cowdung mixture as Influenced by sunlight and shade

Sunlight has got a pronounced influence on gas production characteristics of salvinia as may be observed from the Table 10 and F ig,18. Daily observations are given In Appendix VII.

A perusal of the data clearly indicated that the microbial activity and gas production process is positively influenced by sunlight. 3he time taken for initial gas production was five days under direct sun against sis days in shade. Shis may be due to the favourable temperature conditions for microbial growth under direct sun which inturn is reflected as the reduced lag phase of microbial- growth. The favourable effect of temperature on solubilizing the

 $\label{eq:2.1} \frac{1}{2}\sum_{i=1}^n\frac{1}{2}\sum_{i=1}^n\frac{1}{2}\sum_{i=1}^n\frac{1}{2}\sum_{i=1}^n\frac{1}{2}\sum_{i=1}^n\frac{1}{2}\sum_{i=1}^n\frac{1}{2}\sum_{i=1}^n\frac{1}{2}\sum_{i=1}^n\frac{1}{2}\sum_{i=1}^n\frac{1}{2}\sum_{i=1}^n\frac{1}{2}\sum_{i=1}^n\frac{1}{2}\sum_{i=1}^n\frac{1}{2}\sum_{i=1}^n\frac{1}{2}\sum_{i=1}^n\$

 $\mathcal{L}^{\text{max}}_{\text{max}}$

 $\label{eq:2.1} \frac{1}{\sqrt{2}}\int_{\mathbb{R}^3}\frac{1}{\sqrt{2}}\left(\frac{1}{\sqrt{2}}\right)^2\frac{1}{\sqrt{2}}\left(\frac{1}{\sqrt{2}}\right)^2\frac{1}{\sqrt{2}}\left(\frac{1}{\sqrt{2}}\right)^2.$

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Table 10 Influence of sunlight and shade on gaa production characteristics of salvinia and cowdung mixture

solids also may be noted from the Table. While considering the fact that the temperature fluctuation between shade and sunny conditions was within $3^{\circ}C \rightarrow 5^{\circ}C$. it may be stated that the microbial/fermentative process is very much sensitive to temperature variations. The role of photo indused (of specific wave length) fermentation/microbial activity say also be a reason for the increased gas production under open conditions.

^•2*7 Gas production characteristics of solvinia and cowdung mixture at pilot plant level using different models

Data on the comparative efficiencies of the biogas generators presented in Table 11 and Fig, **19**, (daily gas production details is given in Appendix VIII) revealed that the maximum gas production was obtained with the KVIC model. a constant pressure generator. The remaining three generator models employing variable gas pressure recorded comparatively lesser gas yields. The decreased gas yield of the variable pressure models may be justified as follows. In these variable pressure models continuous gaa production resulted in increased pressure which in turn increased the solubility of carbondioxide in the slurry leading to a

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Table 11 Comparison of pilot plant generator models vith respect to the gas production characteristics of salvlnia covdung mixture

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pH drop. The reduced pH thus resulted was antagenestlc to the mothanogenas which generally prefers a pH range of 7 to 8.5 .

The efficiency of three variable pressure models employed in the study may be rated in the decreasing order, of the new K.A.U.model, Hagyalekshmi model, followed by horizontal type K. A. U. model. This variation may also be explained in terms of the available volume for gas collection and the relative pressure build \mathbf{h}_0 . Thus, the new K.A.U.model having more volume for gas collection and less pressure build up recorded better gas yield. Similarly the horizontal K.A.U.model having the least volume for gas collection and thereby maximum pressure build up recorded the minimum gas yield.

The varying efficiencies of the variable pressure models may be explained in tenas of the diameter to depth ratio of the generator. Work done at NEERI had shown that the gas production per n^3 of digester capacity was maximum whon the diameter to depth ratio was 1 and 0.66. It was considerably less when the ratio was altered to 1.5 or 0.5 (Sathianathan. 1975). Accordingly the new K. A. U. model and Hhagyolakshmi
model (having a diameter to depth ratio equal to one) *>* yielded better then the horizontal $K_{\bullet}A_{\bullet}U_{\bullet}$ model (having a diameter to depth ratio of 1.5). However it should be noted that the performance of generators having equal diameter to depth ratio also varried and it may be attributed to the factors like pressure build up, solubility of carbondioxide and pH change.

On overall efficiency rating, the KVIC model topped the list of the generators employed in this study. However, it has got the limitation that external pressure has to bo exerted to effect the continuous gas out take.

4.2.8 Effect of pressure on biogas production

The results of the experiment, designed to define the optimum pressure requirement for bio-gas production from salvinla is presented In Table 12 and in Fig. 20." Detailed observations are given in Appendix IX.

From the above data, it may be seen that the pressure has got a definite influence on tho gas production characteristics of salvinia, the trend being a negative correlation between the pressure and **86**

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Pressure applied in cms of water I*.6 cm 11.5 cm 18.5 cm tag period for gas production (days) 5 5 5 Period for maximum gas yield (days) 15 15 15 Peat gas production $(11$ tres $)$ 16.5 15.0 11.6 Cumulative gas produ- ^**63.2** ${\tt ct1}$ on (litres) for 45 days 335.8 2?6.8 Cumulative gas production in litres/ κ g of substrate 9.26 6.72 $5.1^{\frac{1}{4}}$ Gas production in *m^/* kg of **T.S. in 45** days 0.203 0.147 0.112 Gas production in m^3/kg 0.236 0.171 0.131 of V.S.in 45 days

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Table 12 Effect of pressure on bio-gas production

gas yield. These observations are contradictory to the general belief that pressure has no Influence on bio-gas production. However, Babbit and Bauman (1958) havedemarcated the upper limit of pressure for optimum gas production as 15 to 18 cm of water. Based on the present findings it may be stated that the minimum pressure should be recommended for maximum gas production. However the depression of pressure beyond a certain limit will lead to operational difficulties of the generator. Accordingly a compromise in terms of minimum pressure and operational convenience should be resorted to. Eventhough 4.6 cm of vater pressure recorded the maximum gao yield, application of additional pressure remained as a serious sot back. As the pressure was increased to 18.5 cm of water, the gas yield was considerably affected. As the pressure was limited to 11.5 on of water a reasonable gas yield was obtained without much operational difficulty. Accordingly 11.5 cm of water pressure appears to be a compromise recommendation.

Sic negative effect of pressure and gas yield may be due to tho increased carbondioxide in tho slurry resulting in, as a low pH and hence low methanogene activity. It should also be noted that the possibility 89

of the slurry getting wasted (the sluriy which comes up through the gap between the digester and the float being exposed to the aerobic breakdown) is more at increased pressure levels loading to poor gas yield,

 $4.2.9$ Comparison of modified bio-gas generators

An experiment was conducted to study the effect of agitation and recirculation in KVIC model and new KAU model respectively. These results were compared with the KVIC model without agitation, Bhagyel^kehmi model, now KAU model without recirculation and horizonthi KAU model. The results are given in Table 13 and Fig. 21 and Appendix X .

It is evident that by providing agitation, the gas production characteristics were Improved, However agitation had no effect on the initial lag for gas production and the days taken to achieve maximum gaa production, 3ho increased gas production obtained by agitation may be due to the fact that agitation helps the trapped carbondicxide particles to escape to the top of the digester resulting in an increased pH of the slurry, Moreover agitation might have helped to have a uniform slurry and thereby ensuring an intimate contact of the bacteria with the substrate. Another

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Table 13 Comparison of modified biogas generators with other generators

favourable effect of agitation may be to maintain a uniform temperature throughout the slurry and also to break the scum at the top and sludge at the bottom of the slurry. Similar favourable effect of agitation on gas production had been reported by Sierp $(1931)_\bullet$

It uas also observed that recirculation also favoured the bioges production. This effect also may be explained in terms of the factors discussed above. Studies at NEERI also had shown similar effect of recirculation on gas production (Sathienathan, 1975).

Even though agitation and recirculation were found to increase the gas production, both these process were cumbersome, laborious and time consuming. So the final experiment on a possible recommendation of a generator model for bio-gas production from salvinia was restricted to the existing KVIC model.

 4 + 2 +10 Exploring the feasibility of utilising existing KVIC type Gobar gas plant for bio-gas production from salvinla*

The results are outlined in Table 14 , Fig.22 and Appendix XX.

It is evident from ; : Table 14 that at the n peak period of gas production (18 deys after initial **is produced** feeding) 0.46 cubic meter of bio-gas which may be sufficient to satisfy the fuel requirements of on individual per day. If the plant sis® is increased to 8 cubic meter the energy requirement of a family consisting of four members may be fulfilled. This figures are however less when compared with the energy obtainable from a Gobar gas plant running with cowdung from 10 cattles and generator size of nine cubic meter. However the gas yield can be considerably increased by utilizing dry salvinia as the raw material thereby increasing the specific quantity of raw materiel per unit volume of the digester.

$4.2.11$ Economic analysis of the household biogas plant utilizing dry salvinia as the substrate

It Is estimated that a six cubic meter capacity digester can yield 3.7 cubic meter of gas per day utilising dried salvinia as the substrate. Therefore about 1350.5 cubic meter of gas can be produced in one year, thich is equivalent to 808 litres of petrol (it is estimated that one cubic meter of bio-gas is equivalent to 0.598 litre of petrol), the cost of which will come to about &.5250.

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Also it is estimated that one tonne of digested material costs **B.80** (used as a fertilizer). Therefore the total income that can be had from 14 tonnes of substrate in one year is 1120 rupees.

It is estimated that 900 rupees is required for the manual collection of salvinia from one hectare. Asuming an yield of 20 kg of fresh salvinia from one square meter, it is calculated that 0.25 hectare of salvinia cultivation is more than enough for the satisfactory running of a six cubic meter plant (400 kg of fresh salvinia which is equal to 40 kg of dry salvinia). Hence the manuel collecting charges for salvinia collection for 45 days will come to $k_{\ast}225$ and for one year around \approx -1800. Also the cost of construction of a six cubic meter capacity plant will come around \approx 9000.

a) Investment

0ost of Installation of the gas plant and manure pit at the current increased price will be around &.9000 which is breaked up as shown.

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Thus it is seen from the figures that, by establishing a biogas plant of 6 cubic meter capacity utilizing dry salvinia as the substrate, the daily cooking and lighting requirements of a family having $7 - 8$ members can be easily met with. It is also seen that besides meeting the fuel requirements, it also fetches an annual savings of B.2870.

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Summary

SUMMARY AND CONCLUSION

Eio present Investigation *on* *Utilisatlcn o f - Salvinia molesta for bio-gas production was undertaken with the main objective of standardising the condition for maximum bio-gas production from salvinia. The \sim assessment of the existing and newly designed bio-gas generators also formed a part of the present investigation. The experiment was conducted in the Department of Agricultural Engineering, College of Horticulture. Vellanikkara during the year 1982-83. The important findings are summariged as follows.

Salvinia molesta contained 4.57 per cent total solids and 85.9 per cent volatile solids and hence it can be utilised as a potential raw material for bio-gas \pm production.

She drying characteristics of salvinla revealed that drying under sun is faster then drying under shade.

Gas production characteristics of salvinia were as follows. From the sixth day onwards the gas production started and attained the peak value of 112 ml on the 20th day. The major bulk of gas produced was carbondioxide during the period from 6 to 11 days. The

actual methane production was observed from the **11**th day onwards. The rate of gas production was found to decrease from the 20th day onwards and it touched the uneconomic level (36 m) by the 45 th day. However compared to cowdung, gas production from salvinla was less under identical conditions.

Studies on the effect of physical conditions of salvinia viz. as a whole, as chopped and as dried, on gas production Indicated that the chopped salvinla Is superior to the other two physical conditions.

A comparative ©valuation of the gas production $characteristics of solution = covding mixture and$ salvinia - water hyacinth mixture showed that the former was superior to the later.

The lag phase for gas production and the period for maximum gas yield remained insensitive to the three salvinla - cowdung proportions <**1** H), (1 i2), (**2**i**1**) employed in the study. However the ratio 1i1 was found to be better with respect to cumulative gas yield, tho gas production per unit total solids and volatile s olid s .

Of the three dilution factors, the substrate $(salylnta + cowdung)$ with water in the ratio 1:1 recorded maximum daily gas yield, cumulative gas yield and gas production per unit total solids and volatile solids over the other two ratios of 2:1 and 1:2.

Sunlight was found to have a pronounced influence on the gas production characteristics of salvinia.

The results obtained with four generator models revealed the superiority of the KHC model, a constant pressure generator over the other three models applying variable pressure viz. New KAU model, Hagyalakahmi model and Horisontal type KAU model.

The study on the effect of pressure on gas production Characteristics of salvinla revealed that the pressure has got a definite influence on the gas production characteristics, the trend being a negative correlation between tho pressure and gas yield.

The *effect* of agitation in KVIC model and recirculation of bio-gas in Naw KAU model showed favourable results. However certain serious set backs

(the process being cumbersome, laborious and time consuming), of these modifications had been identified.

Testing of the existing type KVIC Gobar gas plant (2 cubic meter capacity) with salvinia and cowdung mixture as the raw material revealed that it could be utilized for the daily fuel requirements for cooking and lighting of a single a person.

The design of a prototype unit that could be used for household purposes showed that this requires 6 cubic meter capacity to meet the daily fuel require. ments of $7 - 8$ persons using dried salvinia as the substrate, the loading rate being 40 kg of dried salvinia daily, which can be obtained from drying 400 kg of fresh salvinia.

The economics worked out in this connection revealed that a 6 cubic meter bio-gas plant utilizing dried salvinia as the substrate will be able to fetch an annual income of z .2870 besides meeting the daily fuel requirements.

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References

REFERENCES

Aboaba, F.O., Bruhn, H.D., Koegel, R.G. and Livermore, D.F. 1972. Some fundamental principles of devatering aquatic vegetation. Transaction of $A_2S_4A_6E_6$ $\underline{16}$, $430-434$.

Anon, 1982. A low cost biogas plant uses low density polythene dome, Inversion Intelligence 17 (3): 7.

*Babbit, Bauman. 1958. Severage and Sewage Treatment Wiley, Publishers, p.581.

*Boshoff, 1963. Methane gas production by Batch and
continuous fermentation methods, Tropical Science, **5** (3): 155.

*Boyd, C.F. 1972. A bibliography of interest in the utilisation of aquatic plants. Econ. Bot.
26. (quoted by Mitchell D.S. (Ed), 1974).

Bruhn, H.D., Livermore, D.F., Aboaba, F.O. 1971.
Processing characteristics of macrophytes as related to mechanical harvesting, Trang. An. Sac. Askic. Engrs. 14, 1004-8.

Calicut University, 1979. Ecological survey on African Payal (1978-79). Unpublished report
communicated as per letter No.43168/NCA-3-
78/AD dated 27, 12, 1979 of the Under Secretary (NCA), Dept. Govt. of Kerala, Trivandrum do the Registrar, K.A.U.

Cook, CDK and Gut, B. 1971. Unpublished report on the Salvinia (African Payal) Problem in Kerala. Botenischer Gerten Der Universitat, Lurich, Switzerland.

 104

*Evans, G.C. 1972. The quantitative analysis of plant grouth. Oxford, Blackwell Sci. Publ. (734 D. (Quoted by Mitchell (Ed), 1974).

*Fang, 1973. Methane production from Animal wastes by
Anaerobic Decomposition (Thesis) University of Manitoba/cited in shadduck, Moore, 1975. $50 - 362.$

*Gaudet, J.J. 1973. Growth of a floating aquatic weed, Salvinia, under standard conditions. Evdrobiologea 42: 77-106. (Quoted by Mitchell (Ed) 774 & Mitchell 1976).

George. K. 1976. Studies on the control of some important aquatio weeds of Kerala - Salvinia. Ludwigia and Cyperus. In (Varshney, C.K. (Ed) 1976).

George, K. 1977. The Salvinia weed problem in Kerala. Factors affecting growth and methods of control. In programme & Abstracts of papers. Maed Science conference and Workshop in

Guha, B.R., Bandyopaihyay, T.K., Choudhary, K.K.1976.
Fuel gas and compost manure from water -Hyacinth. Durgapur (West Bengal) Personal communication.

*Hattingh, E. 1961. Problems of Salvinia auriculata Aubl and associated aquatic weeds an Kariba Lake. Weed Research I, 303-306 (Quotod by Sculthorpe, 1967). Ä.

*Holm, L.G., Weldon, L.W. and Black burn, R.D. 1969.
Aquatic weeds Science 166, 699-709.
(Quoted by Mitchell (Ed) 1974).

Ignatious D. Konikkara, 1979. Preliminary work reports. Ph.D. Studies. Calicut University. Botany Dept.

Jayakumar, T.G. 1980. Save Kuttanadu from weeds. Indian Express - Sunday Standard. Daily, 2-3-1980. Madras.

- Joy. P.J. 1978. Ecology and control of Salvinia (African Payal). The molesting weed of Kerala. Kerala Agricultural University, pp.80.
- Kaul, V., and Usha Bakaya, 1976. The noxious floating,
lemid Salvinia aquatic weed complex in Kashmir. In (Varshney, C.K. (Ed), 1976).
- *Little, E.C.S. 1966. The invasion of man-made lakes by plants. Man-made Lakes, Academic Press, Iondon, 75-86.
	- Little, E.C.S. (Ed), 1968. Handbook of Utilization of aquatic plants. F.A.O., United Nations, Roma, pp.123.
- *Little, E.C.S. 1969. Weeds and men-made lakes. Man-made Lakes, The Acera Symposium University Press,
	- Livermore, D.F. and Winderfinch, W.E. 1969. Mechanical removal of organic production from water ways. Eutroplication: causes, consequences, cerraction. National Academy of Sciences, Washington. 494-519 (Quoted by Mitchell (Ed) $(197.)$.
- Livermore, D.F., Bruhn, H.D. and Pollock, B.W. 1971. Processing characteristics of sub surface mactophytes of Modison, Wisconsin Lakes.

*Loyal, D.S. and Crewal, R.K. 1966. Cytological study on sterility in <u>Selvinia curiculata</u> Aubl with a bearing on its reproductive mechanism. Cytologia, 31, 330-8 (quoted by Sculthorpe, 1967).

Mathew, 1980. Estimate of African Payal infestation in Kerala, Direct information from Department of Agriculture, Vikas Haven, Trivandrum,

Menon, M.V.K. 1971, The threatening weeds. Science $20 days, 6 (2) 33-38.$

*Mitchell, D.S. 1970. Autocological studies of Salvinia curiculate. Ph.D. Thesis, University of London. (Quoted by Mitchell (Ed) 1974).

- *Mitchell, D.S. 1973a. The Kariba weed: Salvinia molesta. Brit. Ferngaz. 10: 251-2. (quoted by Joy,
- *Mitchell, D.S. 1973b. Aquatic weeds in man-made lakes. (Geophysical Honosraph Series, 17: 606-611).
(Quoted by Joy, P.J. 1978).
- Mitchell, D.S. 1974a. The development of excessive
populations of aquatic plants. In (Mitchell $D_{\bullet}S_{\bullet}(\text{Ed})$ (1974).
- Mitchell, D.S. 1974b. Environmental management in relation to aquatic weed problems. In <u>Mitchell, D.S</u>. (Ed.) (1974) .
- Mukhopadhyay, S.K. and Taraphdar, S.K. 1976. Aquatic weed problems in West Bengal and control through herbicides. In (Varshney, C.K. (Ed) (1976). i.

끺

National Academy of Science, 1976. Making aquatic weeds useful. Some prospectives for developing Countries. Washington, D.C.

*Penfound, W.T., Earle, T.T. 19+8. The biology of the *Penfound, W.T., Earle, T.T. 19+8. The biology of the (quoted by Mitchell (Ed), 19747.

Robson, 1976. A review of the distribution of aquatic weeds in the Tropics and Sub Tropics. In (Varshney C_eK_e (Ed), 1976).

Samuel, J. 1972. Control of floating type aquatic weeds. A proposed programme of research seminar presented in the Division of Agrl. Engineering. IARI, New Delhi, Nov. 1972.

Samuel, J. and Jippu Jacob, 1977. Prospects for mechenical control of Salvinia in Kerala. Paper presented in the symposium on Rice Research at the Rice Research Station, Pattambi, Kerala, Dec. 1977.

Samuel, J. 1980. Development of Salvinia Harvesting Machine. Paper presented at the seminar, held at the College of Agri., Vellayani, Keyala, Dec. 1980.

Samuel, J., Roy Sukumaran and Kabir Rawther, 1980. Note on Biogas production from African Payal.

Semuel, J. 1981. Personal communication.

'Sathianathan, M.A. 1975. In Bio-gas Achievements and Challenges. 1gt Edn. pp. 14-42. Association of voluntary Agencies for Rural Development - Kailash Colony, New Delhi.

108

Scuthorpe, C.D. 1967. The Biology of acuatic vescular plants. Edward Arnold Ltd., London pp.610.

*Sierp, 1931. The effect of sludge circulation in Digestion tanks on gas production, sludge capacity and seum, abstract/SWJ, 3 (1):154.

Sriramulu, N. and Bhargava, B.N. 1980. Waterhyacinth as a source of energy. Energy menagement. 31 265-73.

Stoner, C.H. 1976. Methane Gas Digesters for fuel and fertilizer - (in producing your own power).
Rudale Press, Inc, Book Division, Emmaus, PA, 8th Ed. pp. 137-176.

*Thomas, C.T., Dovassia, P.A., Kunjikutty, N. and
Mandakumar, N. 1976. A preliminary study
on the chemical composition of African Payal (Salvinia molesta Mitchell) (unpublished) (Quoted by Joy 1978).

Thomas, K.J. 1976. Studies on the aquatic vegetations of Trivendrum (Kerala), In (Vershney, C.K. (Ed) (1976).

Thomas, K.J. 1977. Impact of aquatic weeds on the changing pattern of ecosystem. Proc. All Indian Symp: on Environ. Biol. Univ.

Thomas, K.J. 1979. The extent of Salvinia infestation in Kerala (8.India). Its impact and suggested methods of control. Environmental conservation, Switzerland 6 (1).

109

Ś.

V11

Varghese, P.C. 1974. African Payal, Kalpadhenu, Jan - Feb. 1974, KAU, TWM.

Varshney, C.K. and Singh, K.P. 1976. A survey of aquatic weed problem in India. In (Varshney, C.K. (Ed) 1976).

é, ***Williams, R.H. 1956.** Salvinia auriculata Aublet.
The chemical eradication of a serious
aquatic weed in Ceylon. <u>Trop. Agric</u>. Trin.
22: 145-157. (Quoted by Joy, 1978).

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Appendices

APPENDIX - I

THE MOST COMMON AQUATIC WEEDS IN INDIA*

- $\mathbf I$ Free floating
	- 1. Eichhornia Crassipes (Water hyacinth)**
	- 2. Salvinia spp: (Waterfern, African payal)
	- 3. Pistia Stratiotes (Water lettuce)
	- 4. Lemnoids (Frogbit)
- II Rooted floating
	- 1. Nymphaea Stellato (Water 1111y)
	- 2. Nelumbo nucifera (Lotus)

III Submerged

- 1. Hydrilla Verticullata (Elodea)
- 2. Vallisneria apiralis (Vallisneria)

IV Emergent

- 1. Typha sp: (Cattails)
- 2. Scirpus (Bus rugh)
- * Source: Varshney & Singh (1976)

**Bracketed names indicate the local/popular names.

$APPRBDX - II$

Gas production characteristics of salvinia and cowdung

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Appendix-II (Contd.)

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APPENDIX - III

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Effect of physical conditions of salvinia on gas production

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35	$12 - 82$	71	69	44	2090	2633	1652
36	$13 + -82$	62	55	28	2153	2688	1680
37	$14 - 82$	61	50	26	$221 +$	2738	1706
38	$15 - -82$	59	64	37	2273	2802	1743
39	$16 - 82$	50	48	28	2325	2850	1771
40	$17 - -82$	42	53	23	2365	2903	$179 +$
$2+1$	$18 - -82$	50	1μ	27	$2 + 16$	29+7	1821
42	$19 - -82$	가	43	38	2449	2990	1859
43	$20 - 82$	40	36	27	2489	3026	1886
\mathbf{h}_{1}	$21 - 82$	38	46	22	2527	3072	1908
15	$22 - 82$	42	39	27	2569	3111	1935

Appendix-III (Contd.)

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APPELDIX - IV

 \sim Effect of raw material combination with salvinia on gas production

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31	$26 - 6 - 82$	78	118	9.	1744	3008	2641
32	$27 - 6 - 82$	87	118	105	1831	3126	2746
33	$28 - 6 - 82$	50	78	62	1881	3204	2808
$3 +$	29-6--62	$7 +$	98	74	1955	3302	2882
35	$30 - 6 - 82$	60	90	76	2015	3392	2956
36	$1 - 7 - 82$	58	86	72	2073	3478	3028
37	$2 - 7 - 82$	64	$g+$	73	2137	3562	3101
38	$3 - 7 - 82$	45	58	45	2482	- 3650	3146
39	$i_{i} = 7 - 62$	35	64	60	2217	3714	3206
$2 - 0$	$5 - 7 - 82$	52	64	60	2269	3778	3266
L_{1}	$6 - 7 - 82$	42	$22-$	51	2311	3822	3317
42	$7 - 7 - 82$	62	50	53	2373	3872	3370
$2 + 3$	$8 - 7 - 82$	10	\mathbf{h}	56	2413	3916	3426
$1.1 +$	$9 - 7 - 82$	58	52	44	$2 + 71$	3968	$3 + 70$
45	$10 - 7 - 82$	32	i_{0}	48	2503	4008	3518

Appendix-IV (Contd.)

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APPENDIX - V

Effect of different proportion of cowdung with salvinia ôn gas production

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Appendix-V (Contd.)

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Appendix-V (Contd.)

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APPENDIX - VI

Gas production characteristics of salvinla - cowdung mixture as influenced by the dilution factor

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Appendix-VI (Contd.)

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$S1.$ No.	Date	Daily gas yield in m. (meen values)		Cumulative gas yield in m. <u>(mean values)</u>	
		Sunlight	Shade	Sunlight	Shade
	2	3	4	5	6
1	$27 - 5 - 82$	\bf{O}	$\mathbf 0$	$\mathbf 0$	\mathbf{Q}
2	$28 - 5 - 82$	$\mathbf 0$	O	0	$\bf{0}$
3	29-5--82	$\mathbf 0$	$\mathbf{0}$	$\mathbf 0$	\bullet
ì,	$30 - 5 - 82$	$\mathbf 0$	0	$\mathbf 0$	0
5	$31 - 5 - 82$	52	$\mathbf 0$	52	$\bf{0}$
6	$1 - 6 - 82$	44	12	96	12
7	$2 - 6 - 82$	83	24	179	36
8	$3 - 5 - 82$	87	22	266	58
9	$4 - 82$	119	-50	385	108
10	$5 - 6 - 82$	102	46	482	154
11	$6 - 6 - 82$	106	50	593	50+
12	$7 - 6 - 82$	110	80	703	284
13	$8 - 6 - 82$	132	9.	835	378
1 ¹	$9 - 6 - 82$	126	100	961	478

Influence of sunlight and shade on gas production characteristics of salvinia and cowdung nixture.

 $APPEIDIX - VII$

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Appendix-TII (Contd.)

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Comparison of pilot plant generator models with respect to the gas production characteristics of salvinia and cowdung mixture.

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Appendix-VIII (Contd.)

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 $\label{eq:2.1} \frac{d\mathbf{r}}{dt} = \frac{d\mathbf{r}}{dt} \left[\frac{d\mathbf{r}}{dt} - \frac{d\mathbf{r}}{dt} \right] \left[\frac{d\mathbf{r}}{dt} - \frac{d\mathbf{r}}{dt} \right] \, .$

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 $\label{eq:2.1} \frac{1}{2} \sum_{i=1}^n \frac{1}{2} \sum_{j=1}^n \frac{$

APPENDIX - IX Effect of pressure on bic-gas production

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 $\label{eq:2.1} \mathcal{L}(\mathcal{L}^{\text{max}}_{\mathcal{L}}(\mathcal{L}^{\text{max}}_{\mathcal{L}}))\leq \mathcal{L}(\mathcal{L}^{\text{max}}_{\mathcal{L}}(\mathcal{L}^{\text{max}}_{\mathcal{L}}))$

 $\label{eq:2.1} \frac{1}{2} \sum_{i=1}^n \frac{1}{2} \sum_{j=1}^n \frac{$

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$APPHIDIX - X$

Comparison of modified bio-gas generators with other generators

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Appendix-X (Contd.)

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 $\label{eq:2.1} \frac{1}{\sqrt{2}}\sum_{i=1}^n\frac{1}{\sqrt{2}}\sum_{i=1}^n\frac{1}{\sqrt{2}}\sum_{i=1}^n\frac{1}{\sqrt{2}}\sum_{i=1}^n\frac{1}{\sqrt{2}}\sum_{i=1}^n\frac{1}{\sqrt{2}}\sum_{i=1}^n\frac{1}{\sqrt{2}}\sum_{i=1}^n\frac{1}{\sqrt{2}}\sum_{i=1}^n\frac{1}{\sqrt{2}}\sum_{i=1}^n\frac{1}{\sqrt{2}}\sum_{i=1}^n\frac{1}{\sqrt{2}}\sum_{i=1}^n\frac$

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 AP FENDIX - XI

Gas production characteristics in the existing KVIC
Gobar gas plant

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Appendix-XI (Contd.)

1	p. 2	3	4
$2+$	$13 - 12 - 82$	0.26	5.84
25.	$14 - 12 - 82$	0.39	6.23
26	$15 - 12 - 32$	0, 38	6.61
27	$16 - 12 - 82$	0.37	6,98
28	$17 - 12 - 82$	0.33	7.31
29	$18 - 12 - 82$	0.37	7,68
30	$19 - 12 - 82$	0,22	7.90
31	$20 - 12 - 82$	$0.3 +$	$8.2+$
32	$21 - 12 - 82$	0.37	8.61
33	$22 - 12 - 82$	0.27	8.88
$3 +$	$23 - 12 - 82$	0,28	9.16
35	$2 - 12 - 82$	0.27	9.43
36	$25 - 12 - 82$	0.28	9.71
37	$26 - 12 - 82$	0.26	9.97
38	$27 - 12 - 82$	0.30	10.29
39	$28 - 12 - 62$	0.17	10.44
40	29-12-82	0, 20	10.64
41	$30 - 12 - 82$	0.14	10.78.
L ₂	$31 - 12 - 82$	0.11	10.89
43	$1 - 1 - 83$	0.18	11.07
հե	$2 - 1 - 33$	0.13	11.20
45	$3 - 1 - 83$	0.15	11.35

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UTILIZATION OF " SALVINIA MOLEST ** *(g f iu c t n p a y a l J* **FOR BIO - GAS PRODUCTION

By S. SOMASHEKAREN NAIR

ABSTRACT OF THE THESIS

Submitted in partial fulfilment of the requirement for the degree of

Master of Science in Agricultural Engineering

Σ,

Faculty of Agriculture Kerala Agricultural University

Department of Agricultural Engineering COLLEGE OF HORTICULTURE Vellanikkara - Trichur

ABSTRACT

An investigation on 'Utilization of <u>Salvinia</u> molosta (African Payal) for bio-gas production^{*} was conducted in the Agricultural Engineering Department. College of Horticulture, Kerala Agricultural University with the objective of standardizing the conditions and identifying the best generator model for optimum gas production from salvinla.

From the physical and the gas production characteristic studies, salvinla was recognised as a potential raw material for bio-gas production. For the pilot plant experiments a new design was fabricated and was compared with the adaptive designs of $K_\bullet V_\bullet I_\bullet C_\bullet$ model, Bhagyslekshmi model, and horizontal type K.A.U. model.

Based on the detailed study the conditions for maximum gas yield from salvinia were identified as follows. Chopping, mixing salvinia with cowdung in the ratio 1:1 in terms of dry weight and dilution of substrate to water in the ratio 1:1 in terms of net weight, under sunlight, under low pressure conditions uere identified as the best conditions for obtaining maximum gas yield.

The test conducted in order to find the best design, so as to evolve maximum gas production from salvinia revealed that K.V.I.C. design with agitation and Hew K*A.U, design with recirculation of **blo-ges** were superior to all other models under study $v1x$. **** Hnagyalekshmi model, Horizontal type K.A.U. model etc. However the process of agitation and bio-gas recirculation were identified to be cumbersome, laborious etc. Hence the recommendation of salvinla bio-gas plant may be done for the conventional type **K.V.I.C.** design or for the New K.A.U.design.

The economics worked out for a prototype household type bio-gas plant using dry salvinla ae the substrate having six cubic meter capacity indicated an annual income of \mathbb{S}_4 2870 besides providing the daily fuel requirements.

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